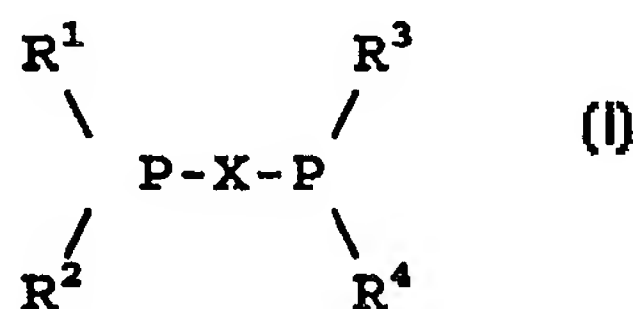




## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

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<b>(21) International Application Number:</b> PCT/NL98/00192 <b>(22) International Filing Date:</b> 6 April 1998 (06.04.98) <b>(30) Priority Data:</b> 97201038.3 7 April 1997 (07.04.97) EP <i>(34) Countries for which the regional or international application was filed:</i> NL et al.  <b>(71) Applicant (for all designated States except US):</b> DSM N.V. [NL/NL]; Het Overloon 1, NL-6411 TE Heerlen (NL).  <b>(72) Inventors; and</b> <b>(75) Inventors/Applicants (for US only):</b> SIELCKEN, Otto, Erik [NL/NL]; Vliekstraat 4, NL-6136 BG Sittard (NL). OEVERING, Henk [NL/NL]; Burg Eussenstraat 46, NL-6181 BR Stein (NL). AGTERBERG, Frank, Petrus, Willibrord [NL/NL]; Geldersoverkwartier 9, NL-6118 EH Susteren (NL). BUIJSEN, Paulus, Franciscus, Anna [NL/NL]; Hoofdstraat 11, NL-6075 AE Herkenbosch (NL). TOTH, Imre [NL/NL]; Rennebeek 42, NL-6166 GM Geleen (NL).  <b>(74) Agent:</b> KLEIBORN, Paul, Erik; Octrooibureau DSM, P.O. Box 9, NL-6160 MA Geleen (NL).		<b>(81) Designated States:</b> AL, AU, BA, BB, BG, BR, CA, CN, CU, CZ, EE, GE, HU, ID, IL, IS, JP, KP, KR, LC, LK, LR, LT, LV, MG, MK, MN, MX, NO, NZ, PL, RO, SG, SI, SK, SL, TR, TT, UA, US, UZ, VN, YU, ARIPO patent (GH, GM, KE, LS, MW, SD, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG).  <b>Published</b> <i>With international search report.</i>

(54) Title: CARBONYLATION CATALYST SYSTEM



## (57) Abstract

Catalyst system comprising a palladium compound, an acid compound having a  $pK_a > 2$  measured in water of 18 °C and a non-symmetrical bidentate phosphorous ligand according to formula (I) in which the  $-PR^1R^2$  group is different from the  $-PR^3R^4$  group and in which X is a divalent organic bridging group, in which the shortest direct link between the two phosphorous atoms in the bridging group X consists of a chain of 2–10 carbon atoms and optionally a sulphur or oxygen atom.

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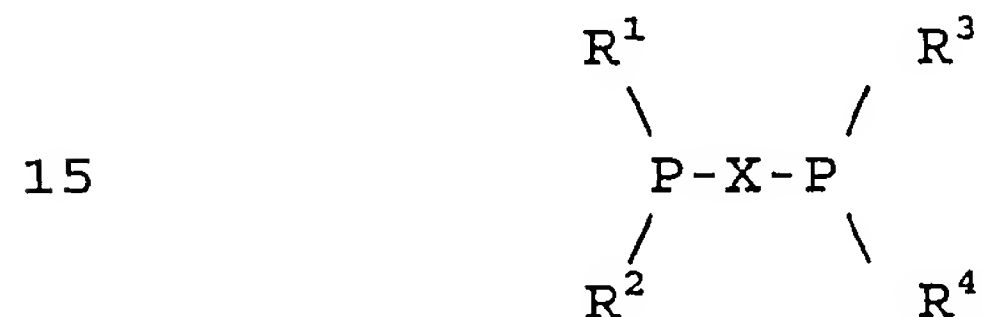
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CARBONYLATION CATALYST SYSTEM

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The invention relates to a novel catalyst system comprising a palladium compound, an acid compound having a  $pK_a > 2$  measured in water of 18°C and  
10 an non-symmetrical bidentate phosphorous ligand according to:



in which the  $-PR^1R^2$  group is different from the  $-PR^3R^4$   
20 group,  $R^1-R^4$  are organic groups and X is a divalent organic bridging group, in which the direct link between the two phosphorous atoms in the bridging group X consists of a chain of 2-10 carbon atoms and optionally a sulphur or oxygen atom.

25 In EP-A-273489 catalyst systems are described comprising palladium, a sterically hindered benzoic acid and a bidentate phosphine, i.e. 1,4-bis(diphenylphosphino)butane for use as catalyst in the carbonylation reaction of conjugated dienes and an  
30 alcohol to alkyl pentenoate compounds.

A disadvantage of this known catalyst composition is that the rate of reaction is relatively low when used as carbonylation catalyst. A need exists for a catalyst system which can increase the rate of  
35 this reaction (at a given temperature). Higher reaction rates also make it possible to operate at lower temperatures. This is advantageous because at lower

temperatures less degradation of the catalyst system takes place. We have found that by using the catalyst system according to the invention the rate of the reaction can be improved considerably.

5           A catalyst system comprising palladium, an acid and non-symmetrical bidentate phosphine ligands, 1-(diisopropylphosphino)-1'-(phenylisopropylphosphino)-ferrocene is described in WO-A-9506027. This publication does not teach in any way that by using  
10 this non-symmetrical phosphine ligand higher reaction rates were to be expected. Moreover, only symmetrical phosphines were used in the examples. Furthermore it has been found that the disclosed catalyst system is less stable than the catalyst system according to the  
15 invention when used in a carbonylation reaction.

The non-symmetrical phosphine can be prepared by well known methods as for example described in GB-A-2101601.

Without being limited to the following theory  
20 it is believed that the improved reaction rate results from the fact that the electronic properties of the two phosphorous atoms of the ligand are different as a result of the different groups bonded to the phosphorous atoms. A larger difference in electronic  
25 properties of the two phosphorous atoms would result in a higher rate of reaction. Therefore it is preferred that one phosphorous atom is substituted with one or two electron withdrawing groups ( $R^1$ ,  $R^2$ ) while the other phosphorous atom is substituted with one or two  
30 electron donating groups ( $R^3$ ,  $R^4$ ). For example  $R^1$ ,  $R^2$  and  $R^3$  can be electron withdrawing groups while  $R^4$  is an electron donating group. This effect can also be achieved when for example  $R^1$  and  $R^2$  are one divalent organic group while  $R^3$  and  $R^4$  are both monovalent

organic groups. More preferably one phosphorous atom is substituted with only electron withdrawing groups while the other phosphorous atom is only substituted with electron donating groups. Examples of electron withdrawing groups are aryl groups optionally substituted with -F, -Cl, -Br, -I, -CF<sub>3</sub>, -SO<sub>3</sub>H, -NR<sup>3+</sup>, -NO<sub>2</sub>, -ONO<sub>2</sub>, -CO<sub>2</sub>H, -CO<sub>2</sub>R, -C(O)R, -NO and -ONO groups (R = C<sub>1</sub>-C<sub>28</sub> alkyl group), or -O-R<sup>5</sup> groups, in which R<sup>5</sup> is preferably an aryl group optionally substituted with the above described groups. Examples of electron donating groups are optionally substituted alkyl groups. Substituents of the alkyl groups is for example a -OR<sup>6</sup>-group, in which R<sup>6</sup> is an C<sub>1</sub>-C<sub>28</sub> alkyl group. Divalent cyclic alkylene groups are also examples of electron donating groups, provided that the number of C-atoms in the ring is equal or higher than 4.

Preferably optionally substituted C<sub>1</sub>-C<sub>10</sub> alkyl groups are used as electron donating groups and optionally substituted C<sub>6</sub>-C<sub>10</sub> aryl groups are used as electron withdrawing groups. Examples are methyl, ethyl, propyl, isopropyl, cyclopropyl, butyl, isobutyl, tert-butyl, cyclobutyl, pentyl, neopentyl, cyclopentyl, hexyl, cyclohexyl, heptyl, cycloheptyl, octyl, cyclooctyl, nonyl, decyl, 2-cyanoethyl, 2-hydroxyethyl, 2-dialkylaminoethyl, 2-bromomethyl, vinyl, allyl, crotyl, phenyl, o-tolyl, p-tolyl, 1-methoxyphenyl, 2-methoxyphenyl, 3-methoxyphenyl, 1-fluorophenyl, 2-fluorophenyl, 3-fluorophenyl, pentafluorophenyl, 2,3-dimethylphenyl, 2,4-dimethylphenyl, 2,5-dimethylphenyl, 2,6-dimethylphenyl, 3,5-dimethylphenyl, 2,4,6-trimethylphenyl, 1-cyanophenyl, 2-cyanophenyl, 3-cyanophenyl, 1- $\alpha,\alpha,\alpha$ -trifluorotolyl, 2- $\alpha,\alpha,\alpha$ -trifluorotolyl, 3- $\alpha,\alpha,\alpha$ -trifluorotolyl, naphthyl and

benzyl. These alkyl groups and aryl groups are optionally (further) substituted with for example methyl, methoxy, cyanide or trifluoromethyl groups.

The bridging group X can be an organic group having between 2 and 20 carbon atoms with the proviso that the shortest direct link between the phosphorous atoms consists of 2 and 10 atoms. Preferably the direct link between the two phosphorous atoms in the bridging group X consists of a chain of 3-4 carbon atoms and optionally an additional non-terminal sulphur or oxygen atom.

Examples of possible non-symmetrical bidentate phosphine ligands are:

1-(diisopropylphosphino)-4-(diphenylphosphino)butane,  
15 1-(dibutylphosphino)-4-(diphenylphosphino)butane,  
1-(dicyclohexylphosphino)-4-(diphenylphosphino)butane,  
1-(ditert-butylphosphino)-4-(diphenylphosphino)-butane,  
1-(tert-butylphenylphosphino)-4-(diphenylphosphino)-  
butane, 1-(butylphenylphosphino)-4-(diphenylphosphino)-  
20 butane, 1-(4,8-dimethyl-2-phosphabicyclo[3.3.1]nonane)-  
4-(diphenylphosphino)butane, 1-(9-bicyclo-  
phosphanonanyl)-4-(diphenylphosphino)butane,  
1-(diisopropylphosphino)-3-(diphenylphosphino)propane,  
1-(ditert-butylphosphino)-3-(diphenylphosphino)-propane  
25 or, 1-(cyclohexylphenylphosphino)-3-(diphenyl-  
phosphino)-propane.

The palladium can be present in the catalyst system in the form of a heterogeneous palladium compound or as a homogeneous palladium compound.

30 Homogeneous systems are preferred. Since palladium forms complexes with the phosphine ligand, the choice of the initial Pd compound is in general not critical. Homogeneous palladium compounds include, for instance, palladium salts of, for instance, nitric acid,



5 sulphonic acid, alkane carboxylic acids with not more than 12 carbon atoms or hydrogen halogenides (Cl, Br, I). Metallic palladium can also be used. Exemplary homogeneous palladium compounds include  $\text{PdCl}_2$ ,  $\text{PdBr}_2$ ,  $\text{PdI}_2$ ,  $\text{Na}_2\text{PdI}_4$ ,  $\text{K}_2\text{PdI}_4$ ,  $\text{PdCl}_2(\text{benzonitrile})_2$  and bis(allylpalladium chloride). Another group of suitable halogen-free palladium compounds are palladium complexes such as palladium acetylacetonate ( $\text{Pd}(\text{acac})_2$ ),  $\text{Pd}(\text{II})$ acetate, palladiumnitrate  $\text{Pd}(\text{NO}_3)_2$ , tris(tri-o-  
10 tolyl phosphine) palladium, and di-palladium-tris-(dibenzylideneacetone) ( $\text{Pd}_2(\text{dba})_3$ ). An exemplary of a heterogeneous palladium compound is a palladium compound on an ion exchanger such as, for example an ion exchanger containing carboxylic acid groups. Ion  
15 exchangers containing carboxylic acid groups are commercially available under the brand names Amberlite IRC 50 and Amberlite IRC 84 (Rohm & Haas). Another heterogeneous catalyst is an immobilized phosphine on carrier catalyst, in which the palladium forms  
20 complexes with the immobilized phosphine (phosphine being the ligand of the catalyst system). Carriers include polystyrene, polyacrylamide, silica, alumina, silica-alumina or zeolite support.

The acid compound with a  $\text{pK}_a > 2$  is generally  
25 a protonic acid, preferably having a  $\text{pK}_a$  between 2-6 measured in water at  $18^\circ\text{C}$ . Preferred acids are carboxylic acids having 1 to 30 carbon atoms. These carboxylic acids may be substituted with hydroxy,  $\text{C}_1\text{-C}_4$  alkoxy groups, for example methoxy, amine or halogenide  
30 groups, for example Cl, I and Br. Exemplary carboxylic acids are benzoic acid, acetic acid, valeric acid, pentenoic acid, nonanoic acid and butanoic acid. The acid is preferably a sterically hindered carboxylic acid having a  $\text{pK}_a$  of less than 4.5. Exemplary

sterically hindered carboxylic acids are sterically hindered benzoic acids, for example 2-fluorobenzoic acid and 2-(trifluormethyl)-benzoic acid, the C<sub>1</sub>-C<sub>4</sub> alkyl substituted benzoic acid, for example 2,6-dimethylbenzoic acid, 2-methylbenzoic acid, 2,4,6-trimethyl benzoic acid and hydroxy substituted benzoic acid, for example meta- and parahydroxybenzoic acid and other substituted benzoic acids, for example 2,6-difluorobenzoic acid or 2,4,6-tribromobenzoic acid.

10 Most preferably 2,4,6-trimethylbenzoic acid is used.

The molar ratio of acid to palladium is preferably between 6:1 and 50:1 and more preferably between 10:1 and 40:1. It has been found that the optimum acid to palladium ratio depends on the specific carboxylic acid which is used.

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The phosphine ligand to palladium molar ratio is as a rule between 1:1 and 100:1 and preferably between 2:1 and 10:1.

The palladium concentration in the reaction mixture is preferably as high as possible because the rate of the reaction per unit of reactor volume will then be higher. The upper limit for a homogeneous catalyst system will normally be determined by the solubility of palladium in the reaction mixture and will, for example, depend on the specific palladium compound used as discussed above. This upper limit can easily be determined by one skilled in the art.

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However, the process according to the invention may also be performed with a homogeneous catalyst system in the presence of additional solid palladium compounds.

The catalyst system according to the invention can be advantageously used as a carbonylation catalyst in a reaction of an olefinic organic compound, carbon monoxide and optionally a co-reactant. The



olefinically unsaturated compound can be a C<sub>2</sub>-C<sub>20</sub> organic compound, for example ethene, propene, butene, pentenes, hexenes and octenes. Preferably a conjugated diene, for example 1,3-pentadiene, 1,3-hexadiene and more preferably 1,3-butadiene is used. The co-reactant is preferably a nucleophilic compound having a mobile H-atom, for example water or a C<sub>1</sub>-C<sub>20</sub> carboxylic acid. More preferably the co-reactant is an alcohol having between 1 and 20 carbon atoms. Examples of suitable alcohols are methanol, ethanol, propanol, isopropanol, n-butanol, tert-butanol, pentanol, cyclohexanol and phenol. Most preferably methanol and ethanol are used, for example because the resulting compounds can be advantageously be used as precursor to prepare nylon intermediates, like adipic acid and ε-caprolactam.

It has been found that this catalyst system according to the invention can also be advantageously used when converting 3-alkoxy-1-butene and/or 1-alkoxy-2-butene to the corresponding alkyl pentenoate. These compounds can be prepared from butadiene as for example described in EP-A-25240. The reaction conditions of the reaction from alkoxy butene to an alkyl pentenoate are generally the same as for the direct carbonylation of butadiene except that no additional alcohol is required as co-reactant.

The catalyst system can also be used as polymerization catalyst in processes to prepare polyketones by co-reacting unsaturated compounds with CO.

The molar ratio of co-reactant and butadiene in the reaction mixture may be between 0.1:1 and 10:1. In a continuous process it is preferred to keep this ratio between 0.5:1 and 3:1. More preferably this ratio is smaller than 1.5:1.

The molar ratio of conjugated diene and palladium can be between 0.01:1 and 1000:1. Preferably this ratio is between 10:1 and 300:1 and more preferably higher than 50:1.

5                   The temperature during the carbonylation reaction is preferably between 25°C and 200°C. The pressure is not particularly critical and generally ranges between 1 MPa and 100 MPa, although it is preferably greater than 2 MPa. An upper limit is not  
10 critical. A very high pressure is disadvantageous because the process equipment will become very expensive. A practical and preferred upper limit is therefore about 10 MPa.

                  The carbon monoxide can be used in a pure  
15 form or diluted with an inert gas such as, for example, nitrogen, rare gases or carbon dioxide. In general, more than 5% hydrogen is undesirable, since this can cause hydrogenation of the olefinic organic compound under the carbonylation conditions.

20                   All inert solvents are in principle suitable as an additional solvent when using the catalyst system in a carbonylation reaction. It is also possible to use an excess of one of the reactants or (by-) products in such an amount that a suitable liquid phase is formed.  
25 Examples of (by-) products when reacting butadiene are C<sub>9</sub>-esters and other high boiling by-products. Examples of inert solvents are sulphoxides and sulphones, such as for instance, dimethyl sulphoxide, diisopropyl sulphone; aromatic solvents, such as benzene, toluene,  
30 xylene; esters, such as methyl acetate, methyl valerate, pentenoate esters and butyrolactone; ketones, such as acetone or methylisobutyl ketone; ethers such as anisole, trioxanone, diphenyl ether and diisopropyl

ether; and mixtures of these solvents. Preferably, diphenyl ether is used as additional solvent.

Preferably a continuous process is used. An example of reactor system for a continuous process is a series of continuously stirred tank reactors (CSTR) in which the catalyst system, a possible solvent, olefinic organic compound, optionally the co-reactant and carbon monoxide are fed to a first reactor. The various ratios according to the process of the invention can be maintained by controlling the feed rate of the various reactants and catalyst components.

The invention shall be elucidated by the following non-limiting examples.

15 Example I

A 160 ml autoclave was filled with 0.133 grams (0.6 mmol) palladium acetylacetonate, 1.982 grams (1.2 mmol) 2,4,6-trimethylbenzoic acid and 3.0 mmol of a bidentate phosphine ligand (see Table 1). The autoclave was purged three times with nitrogen. Subsequently 75 ml water- and oxygen-free diphenylether was injected. The autoclave was purged three times with carbon monoxide before adjusting the pressure to 2.0 MPa with a CO atmosphere and subsequently the temperature was raised to 140°C. Immediately after reaching this temperature a mixture of 6.5 grams of butadiene, 4.0 grams methanol and 0.5 grams nonane (internal GC standard) was injected with CO into the autoclave. After injecting these starting compounds the pressure was adjusted to 5.0 MPa using CO. After the reaction time (see Table) the reaction mixture was analyzed by Gas Chromatography (GC). The results are presented in Table 1.

TABLE 1

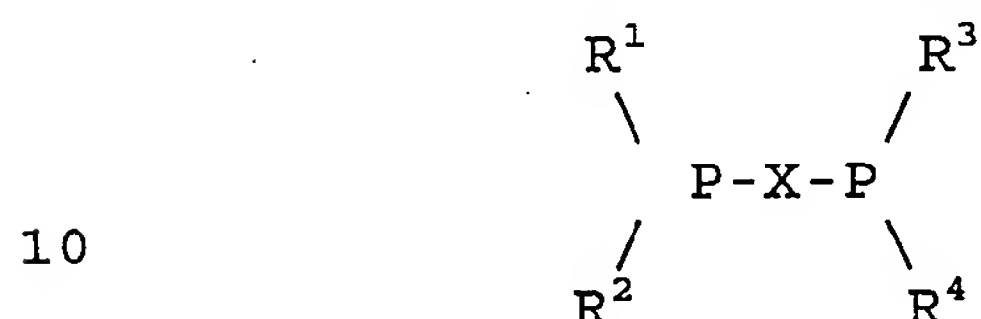
Example	ligand	reaction time (hours)	selectivity (a) (%)	conversion (%)	relative reaction rate (b)
I	1-(di-isopropylphosphino)-4-(diphenylphosphino)butane	1.5	86.1	87	1.75
II	1-(dibutylphosphino)-4-(diphenylphosphino)butane	0.5	91.7	45	1.5
III	1-(butylphenylphosphino)-4-(diphenylphosphino)butane	1.0	92.9	62	1.25
IV	1-(4,8-dimethyl-2-phosphabicyclo[3.3.1]nonanyl)-4-(diphenylphosphino)butane	1.5	89.9	81	1.43
V	1-(tert-butylphenyl-phosphino)-4-(diphenylphosphino)butane	1	95.6	60	1.14
comp A	1,4-bis-(di-isopropyl-phosphino)-butane	1.5	88.7	49	0.55
comp B	1,4-bis-(isopropylphenyl-phosphino)-butane	0.75	90.0	32	0.63
comp C	1,4-bis-(diphenyl-phosphino)butane	1.0	92.9	56	1

(a) Selectivity to methyl pentenoate  
(b) The reaction rates were normalized to the reaction rate of bis-(diphenylphosphino)butane (Comparative Experiment C; relative reaction rate = 1)

- 11 -

C L A I M S

1. Catalyst system comprising a palladium compound, an acid compound having a  $pK_a > 2$  measured in water of 18°C, and a non-symmetrical bidentate phosphorous ligand according to:



in which the  $-PR^1R^2$  group is different from the  $-PR^3R^4$  group and in which X is a divalent organic bridging group, in which the shortest direct link between the two phosphorous atoms in the bridging group X consists of a chain of 2-10 carbon atoms and optionally a sulphur or oxygen atom.

2. Catalyst composition according to claim 1, characterized in that  $R^1$ ,  $R^2$  are electron withdrawing groups and  $R^3$  and  $R^4$  are electron donating groups.
3. Catalyst composition according to claim 2, characterized in that the electron withdrawing groups are optionally substituted  $C_6-C_{10}$  aryl groups and the electron donating groups are optionally substituted  $C_1-C_{10}$  alkyl groups.
4. Catalyst composition according to claim 3, characterized in that  $R^1$  and  $R^2$  are aryl groups substituted with electron withdrawing groups.
5. Catalyst system according to any one of claims 1-4, characterized in that the direct link between the two phosphorous atoms in the bridging group X consists of a chain of three or four carbon atoms

- 12 -

and optionally a non-terminal sulphur or oxygen atom.

6. Catalyst system according to any one of claims 1-5, characterized in that the acid is a substituted benzoic acid.
7. Use of a catalyst system according to any one of claims 1-6 as a catalyst in a carbonylation reaction of an olefinic organic compound, carbon monoxide and optionally a co-reactant.
8. Use according to claim 7, characterized in that the olefinic compound is 1,3-butadiene and the co-reactant is a C<sub>1</sub>-C<sub>20</sub> alcohol.
9. Use of a catalyst system according to any one of claims 1-6 as catalyst in the reaction between an alkoxy butene and carbon monoxide in a process to prepare an alkyl pentenoate.



# INTERNATIONAL SEARCH REPORT

International Application No  
PCT/NL 98/00192

A. CLASSIFICATION OF SUBJECT MATTER  
IPC 6 B01J31/24 C08G67/02

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)  
IPC 6 B01J C08G

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US 5 350 876 A (DRENT EIT ET AL) 27 September 1994 see column 4, line 16 - line 66 ---	1-9
Y	GB 2 101 601 A (JOHNSON MATTHEY PLC) 19 January 1983 cited in the application see page 10, line 25 - line 26 ---	1-9
A	US 4 818 810 A (DRENT EIT) 4 April 1989 see claim 1 ---	1
A	EP 0 490 452 A (SHELL INT RESEARCH) 17 June 1992 see abstract --- -/--	1,6

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

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Date of the actual completion of the international search

24 June 1998

Date of mailing of the international search report

02/07/1998

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INTERNATIONAL SEARCH REPORT

In	tional Application No
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C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	EP 0 305 012 A (SHELL INT RESEARCH) 1 March 1989 see claim 1 -----	1

# INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/NL 98/00192

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